Appl. No. 10/537,973

Amendment dated June 9, 2008

Applicants' Response to the Office Action mailed December 7, 2007

## In the Claims:

Please amend pending Claim 13, cancel previously presented Claim 24, and add new Claim 26, as shown in the Listing of Claims below, which is a complete listing of all Claims ever presented and replaces all prior versions, and listings, of the Claims in the instant Application.

## Listing of Claims

1-12. (Canceled)

- 13. (Currently amended) A countercurrent process for the continuous esterification of  $C_{1.22}$  fatty acids with  $C_{1.10}$  monoalkanols,  $C_{2.5}$  di- or trialkanols or mixtures thereof, said process comprising
- (a) partially reacting the fatty acids and alkanols in a preliminary reactor in the liquid phase in the presence of an a heterogeneous catalyst selected from the group consisting of organic or inorganic, basic or acidic, anion or cation exchangers, acid clays and zeolites.
- (b) passing the partially-reacted reaction mixture to a separation unit,
- (c) removing water from the partially-reacted reaction mixture in the separation unit,
- (d) passing the resulting de-watered, partially-reacted reaction mixture to a countercurrent reaction column.
- (e) further reacting the fatty acids and alkanols in the countercurrent reaction column in the liquid phase in the presence of heterogeneous catalysts, and
- (f) removing the crude product from the bottom of the reaction column.
- 14. (Previously presented) A process according to claim 13, further comprising increasing the vapour load in the lower part of the reaction column by feeding nitrogen into the reaction column at the lowermost plate.
- 15. (Previously presented) A process according to claim 13, wherein the preliminary reactor is a fixed-bed reactor.

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- 16. (Previously presented) A process according to claim 13, wherein the esterification reaction is carried out at temperatures of 50 to 200°C.
- 17. (Previously presented) A process according to claim 16, wherein the esterification reaction is carried out at temperatures of 80 to 150°C.
- 18. (Previously presented) A process according to claim 13, wherein the fatty acids are esterified with C<sub>1-10</sub> monoalkanols.
- 19. (Previously presented) A process according to claim 18, wherein the fatty acids are esterified with C<sub>1.8</sub> monoalkanols.
- 20. (Previously presented) A process according to claim 18, wherein the fatty acids are esterified with isopropanol or 2-ethylhexanol.
- 21. (Previously presented) A process according to claim 13, wherein the fatty acids are esterified with  $C_{2\cdot 3}$  di- or trialkanols.
- 22. (Previously presented) A process according to claim 21, wherein the fatty acids are esterified with C<sub>2.3</sub> di- or trialkanols.
- 23. (Previously presented) A process according to claim 21, wherein the fatty acids are esterified with glycerol.
- 24. (Canceled)
- 25. (Previously presented) A process according to claim 13, wherein acidic cation exchangers are used as the catalyst.

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26. (New) The process according to claim 13, wherein the heterogeneous catalyst is selected from specially worked-up bleaching earths and catalysts based on transition metals.